

PHASE FORMATION MECHANISM AND KINETICS IN SOLID-STATE SYNTHESIS OF Ba-DOPED YE'ELIMITE: THE EFFECT OF Ba-DOPING CONCENTRATION ON $C_{4-x}B_xA_3$ SYSTEMS

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Calcium barium sulfoaluminate (abbr: $C_{4-x}B_xA_3$), one of the special cementitious minerals originated from ye'elimite (abbr: C_4A_3), has superior hydration and hardening performance. In this paper, a series of $C_{4-x}B_xA_3$ with different Ba-doping concentrations ($x = 0, 0.5, 1, 1.5$ and 2) were prepared, and the effect of the Ba-doping concentration on the formation was systematically investigated by the Rietveld/XRD quantitative phase analysis. The results show that $BaSO_4$ is the essential intermediate phase for the formation of the Ba-doped ye'elimite. The solid-state reaction process of $C_{4-x}B_xA_3$ is separately expressed as two main forms, corresponding to the cases in which the Ba-doping concentration (x) is larger than and less than "1", respectively. The Jander diffusion model shows the optimal fitting for $C_{4-x}B_xA_3$ and it clearly proves that the $C_{4-x}B_xA_3$ formation becomes increasingly difficult as the Ba-doping concentration increases. The correlation between the apparent activation energy (E_a) and the Ba-doping concentration is positively well related, which can be expressed as ' $E_a = 71.9x + 304$ ' ($\text{kJ}\cdot\text{mol}^{-1}$).

INTRODUCTION

Portland cement is one of the most widely used cementitious materials in land-based architectures, underground projects and marine constructions. However, the drawback of poor durability limits its wide application in severe environments, such as high humidity, high saline-alkali and marine environments [1]. In contrast, calcium sulfoaluminate (CSA) cement shows more satisfactory properties and has been well applied to some special projects such as repairing and constructing marine facilities [2, 3]. It has advantages such as higher early strength, faster hardening and better anti-corrosion and anti-permeability properties [4].

The sulfoaluminate ($4\text{CaO}\cdot 3\text{Al}_2\text{O}_3\cdot \text{SO}_3$, abbreviated as C_4A_3 and also named Ye'elimite) as the dominant mineral in CSA, plays a key role in improving the durability in severe environments. It has a sodalite structure with the general composition of $M_4[T_6O_{12}]_X$ where $M=\text{Ca}$, $T=\text{Al}$, and $X=\text{SO}_4$ [5-7]. Such a structure possesses four tetragonal and eight hexagonal axial channels with narrow gaps, paralleled in the direction of [001], which is convenient for reactions with water [8-10]. Although CSA performs well in marine engineering, it has not been considered completely satisfactory to meet the increasingly stringent requirements of

modern applications. The C_4A_3 modification is a feasible strategy, through which new minerals of $C_{4-x}B_xA_3$ by barium incorporation have been proven particularly successful in improvement of the performance. $C_{4-x}B_xA_3$ has a similar crystal structure, but much higher early strength and better stability [11, 12]. The study of the formation process is the first and most important step to understand $C_{4-x}B_xA_3$. The general solid-state reaction of C_4A_3 can start from $950\text{ }^\circ\text{C}$, can form in substantial amounts between $1300 - 1350\text{ }^\circ\text{C}$ and can decompose when the temperature further rises beyond $1350\text{ }^\circ\text{C}$ [13, 14]. When Ba is doped, $C_{4-x}B_xA_3$ minerals have a similar formation process and usually form in substantial amounts when the sintering temperature goes higher than $1350\text{ }^\circ\text{C}$ [15-17]. In addition, more and more researchers have reached an agreement that Ba^{2+} substitution at the Ca^{2+} -site in C_4A_3 had a positive effect on increasing its decomposition temperature [18-20]. Cheng [12] prepared a series of $C_{4-x}B_xA_3$ minerals ($0 \leq x \leq 3$) and demonstrated that $C_{2.75}B_{1.25}A_3$ showed the most satisfactory mechanical property. Lu and Chang [20-24] conducted a more detailed study on the formation process of the $C_{2.75}B_{1.25}A_3$ mineral and obtained the best calcination system of $C_{2.75}B_{1.25}A_3$ minerals.

Although the formation processes of some $C_{4-x}B_xA_3$ minerals such as C_3BA_3 and $C_{2.75}B_{1.25}A_3$ have been

studied already, the formation and decomposition processes of $C_{4-x}B_xA_3$, especially the effect of the Ba-doping concentration on the kinetics of formation, have not been systematically elucidated upon. In this paper, the minerals are prepared according to the molar ratio of $C_{4-x}B_xA_3$ ($x = 0, 0.5, 1, 1.5$ and 2). The formation rate of the $C_{4-x}B_xA_3$ minerals at the different calcination systems are quantified via the Rietveld/XRD method and the comprehensive kinetic of formation is discussed. This study is a step forward to better understanding ye'elimite.

EXPERIMENTAL

Raw materials

The analytical pure reagents of $CaCO_3$, $BaCO_3$, Al_2O_3 and $CaSO_4 \cdot 2H_2O$ (a purity of 99.9 %, from the Sinopharm Chemical Reagent Co., Ltd, China) were used in this work to synthesise $C_{4-x}B_xA_3$. They were ground and sieved through 74 μm prior to being used.

Sample preparation

Mixtures of the stoichiometric proportion of the above chemical reagents were prepared to synthesise $C_{4-x}B_xA_3$, where x was set as 0, 0.5, 1, 1.5 and 2, respectively. The resulting powders were firstly ground in a planetary mill with absolute ethanol at 200 rpm for 30 min and then dried at 50 °C. The powders were finally compressed into thin rectangular samples (40 × 40 × 3 mm) under 12 MPa pressure. The sintering system of the target minerals (C_4A_3 , $C_{3.5}B_{0.5}A_3$, C_3BA_3 , $C_{2.5}B_{1.5}A_3$, and $C_2B_2A_3$) were slightly varied and detailed in Table 1, where the sintering duration (SD) meant the time-period under a certain sintering temperature. A total of 225 samples were scanned under an X-ray diffractometer and finally evaluated by the Rietveld/XRD quantitative analysis.

Table 1. The sintering system design for the target $C_{4-x}B_xA_3$ minerals*.

Ba-doping concentration (mol)	Sintering temperature (°C)	Sintering duration (min)
0	1200	0
0.5	1250	30
1	1300	60
1.5	1350	90
2	1400	120
–	–	240
–	–	480
–	–	720
–	–	1200

* In this experiment design, the 225 samples were obtained through rearranging and combining based on factors of the Ba-doping (5 levels), the sintered temperature (5 levels) and the sintered time (9 levels).

Testing methods

The XRD patterns were recorded in the Bragg-Brentano reflection geometry ($\theta/2\theta$) on a D8 ADVANCE (Bruker AXS) diffractometer. The detailed instrument settings for the XRD are summarised in Table 2. The Rietveld refinement was implemented by using TOPAS 4.2 software. The refined overall parameters were the cell parameters, zero-shift error, background, phase scale and peak shape parameters using the fundamental parameters approach [25-27].

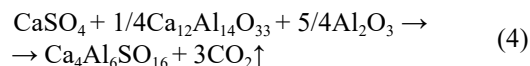
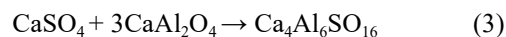
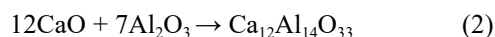
Table 2. The XRD instrument settings.

Parameter	Step scanning
X-ray radiation power	40 kV/40 mA
Wavelength type: $CuK\alpha 1$	$K\alpha 1 = 1.5406 \text{ \AA}$
Detector	X'Celerator detector
Divergence slit (°)	1.00
Soller slit (rad)	0.04
Receiving slit (°)	0.6
Step width (°)	0.02
Measure time (h)	0.5
Scan range ($2\theta / ^\circ$)	5-70

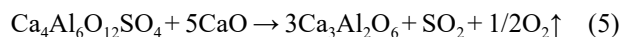
RESULTS AND DISCUSSIONS

Formation Process of $C_{4-x}B_xA_3$ Minerals

A series of $C_{4-x}B_xA_3$ minerals with different Ba-doping concentrations were prepared by solid-state reaction. The XRD qualitative analysis of the samples with the different sintering systems was firstly performed and the selected XRD patterns for the samples sintered at 1300 °C for 4 hours are shown in Figure 1. For C_4A_3 , most diffraction peaks show stoichiometric ye'elimite itself. The formation is mainly governed by Equations (1-4):



Some impurity peaks with very low intensity are detected as $Ca_{12}Al_{14}O_{33}$ ($C_{12}A_7$), $Ca_3Al_2O_6$ (C_3A) and $CaAl_2O_4$ (CA), respectively. For CA and $C_{12}A_7$, the reason is mainly due to the decomposition of a small amount of gypsum, leading to sulfate insufficiency, which has been well accepted already in some previous studies [28-37]. The presence of C_3A here could be attributed as the C_4A_3 decomposition according to Equation (5) [29]:



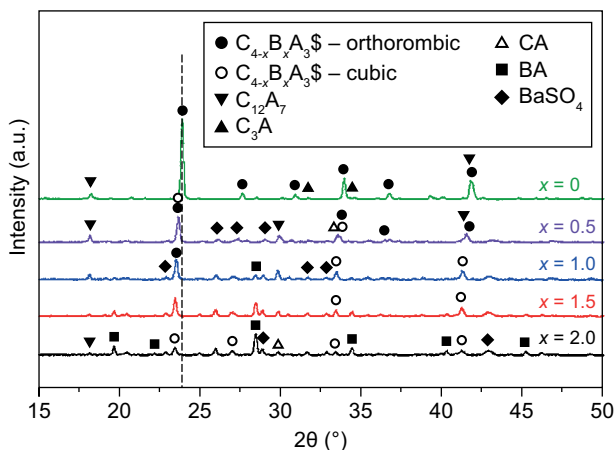


Figure 1. The XRD patterns of the $C_{4-x}B_xA_3$ systems sintered at 1300 °C for 4 h.

When Ba^{2+} is doped, the impurity phase assemblage tends to be complicated, including $BaSO_4$ (BS), $BaAl_2O_4$ (BA), CA and $C_{12}A_7$. BS and BA are formed as the intermediate phases according to Equations (6) and (7), respectively. Based on the analysis of the stoichiometric ye'elimite [31, 32], the formation process of $C_{4-x}B_xA_3$ can be proposed as Equations (8-10), where Equation (8) and Equations (9-10) describe the cases of ' $x < 1$ ' and ' $x > 1$ ', respectively. $BaSO_4$ is preferentially formed no matter how much Ba^{2+} is doped, which is due to its better stability at a high temperature [31]. Also, the peak intensity of $C_{4-x}B_xA_3$ gradually decreases with an increase in the Ba-doping concentration. They both indicate that the solid-state reaction becomes more difficult after the barium incorporation. In addition, the XRD patterns clearly show that the main peak of $C_{4-x}B_xA_3$ ($2\theta = 23.44 - 23.88^\circ$) has a gradual left-shift in the position, which reflects that the cell volume became significantly enlarged based on the barium incorporation. The detailed results are reported in the following Rietveld analysis.

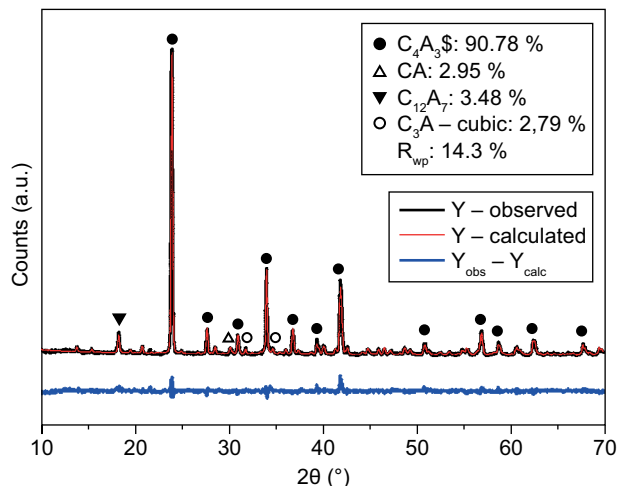
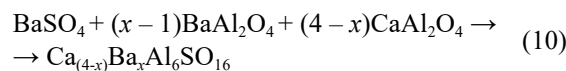
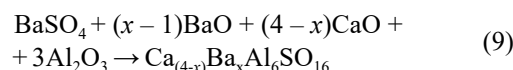
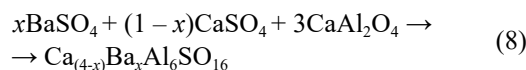


Figure 2. The result of the Rietveld quantitative phase analysis of the C_4A_3 mineral.



The Rietveld quantitative results of the above selected XRD patterns (the $C_{4-x}B_xA_3$ minerals sintered at 1300 °C for 4 hours) are shown in Table 3. Wherein, one representative Rietveld refinement plot of the C_4A_3 sample is shown in Figure 2. Based on the low R_{wp} values ($< 15\%$, the value is the difference between the calculated result via the TOPAS 4.2 software and the observed data) and the smooth difference curve of the Rietveld refinement indicated that the fittings are satisfactory. The quantitative results of $C_{4-x}B_xA_3$ (both orthorhombic and cubic structures) basically follow a decreasing trend

Table 3. The Rietveld quantitative phase analysis of the $C_{4-x}B_xA_3$ samples sintered at 1300 °C for 4 h.

Analysis	Phases and R-factors	C_4A_3	$C_{3.5}B_{0.5}A_3$	C_3BA_3	$C_{2.5}B_{1.5}A_3$	$C_2B_2A_3$	ICSD codes
Quantitative results (wt.%)	Ye'elimite_orthorhombic	90.8(4)	20.8(3)	10.6(3)	10.4(2)	8.9(1)	80361
	Ye'elimite_cubic	–	6.1(3)	21.7(4)	18.1(2)	18.9(2)	81654
	C_3A	2.8(2)	1.2(1)	–	–	–	1841
	$C_{12}A_7$	3.5(2)	27.4(4)	16.5(2)	7.1(1)	6.8(1)	29212
	CA	2.9(2)	36.1(5)	29.7(4)	27.4(3)	27.1(4)	260
	$BaSO_4$	–	6.9(2)	16.7(2)	24.9(2)	25.7(2)	16904
	$BaAl_2O_4$	–	1.5(1)	4.7(1)	12.1(1)	12.6(2)	10036
Cell volume (cm^3)	Ye'elimite_orthorhombic	1.55×10^{-21}	1.56×10^{-21}	1.57×10^{-21}	1.61×10^{-21}	1.61×10^{-21}	–
	Ye'elimite_cubic	–	7.90×10^{-22}	7.91×10^{-22}	8.00×10^{-22}	8.03×10^{-22}	–
Criteria of fit	R_{wp} (%)	14.3	14.8	12.8	13.9	14.1	–

as the Ba-doping concentration increases with the exception of $C_{3.5}B_{0.5}A_3$. That exception is probably due to the current sintering temperature that could not fully satisfy the requirement of the $C_{3.5}B_{0.5}A_3$ formation. Meanwhile, the Ba-doping concentration is not high enough for the sulfur solidification. With the prolonged sintering time, excessive sulfur volatilization from $CaSO_4$ decomposition restricts the formation of ye'elinite. The cell volume of ye'elinite in both the orthorhombic and cubic structures are also reported in Table 3, directly proving the growing tendency based on the barium incorporation. For the impurity phase of C_3A , it decreases gradually and disappears when the Ba-doping concentration is larger than 1.0 ($x > 1$). The Ba-doped ye'elinite has a relatively higher decomposition temperature, which is consistent with the above analysis, indicating that C_3A is mainly from the decomposition process of ye'elinite. As expected, the quantitative results of $BaSO_4$ and $BaAl_2O_4$ show a gradually growing tendency with an increase in the Ba-doping concentration and reaches a stable level with the further addition. The basic trend is consistent with that of 'Ye'elinite_orthorhombic'. However, for 'Ye'elinite_cubic', it shows a slightly lower amount in the sample of $C_{2.5}B_{1.5}A_3$ and $C_2B_2A_3$ compared with that in C_3BA_3 . It again indicates that an increase in the Ba-doping concentration brings more difficulty for the formation of $C_{4-x}B_xA_3$.

Conversion rate of $C_{4-x}B_xA_3$

The conversion rates of the Ba-doped ye'elinite under the individual conditions, versus the temperature, sintering duration and Ba-doping concentration, were determined based on the above Rietveld/XRD quantitative analysis. The results are detailed in Figure 3. For C_4A_3 (Figure 3a), the representative formation process is consistent with previous studies, which provides basic rules for studying the Ba-doped ye'elinite [13, 28, 33-39]. The mass fraction of C_4A_3 gradually increases with the prolonged sintering time. When the temperature is between 1200 °C and 1300 °C, the reaction rate (slope of a certain point) shows a gradually decreasing tendency with a longer sintering duration. This is mainly caused by the slower diffusion in the late stage of the solid-state reaction. In comparison, the effect of the temperature on the conversion rate is more significant than the sintering duration. The conversion rate can reach a completely high level (> 90 wt. %) within a short time (30 - 60 min) above 1350 °C. It indicates that fast sintering at a high temperature is helpful in obtaining C_4A_3 with a high purity. It is noteworthy that the raw materials were calcinated in a relatively closed furnace and that the fast sintering can obviously reduce the harmful effect of the sulfur escape.

The conversion rates of $C_{3.5}B_{0.5}A_3$, C_3BA_3 , $C_{2.5}B_{1.5}A_3$ and $C_2B_2A_3$ under the conditions of the different temperature and sintering duration are plotted

in Figure 3b-e, respectively. As $C_{4-x}B_xA_3$ ($x > 0$) originates from C_4A_3 , they have a similar formation process. However, compared with C_4A_3 , the conversion rate of the Ba-doped ye'elinite is significantly reduced

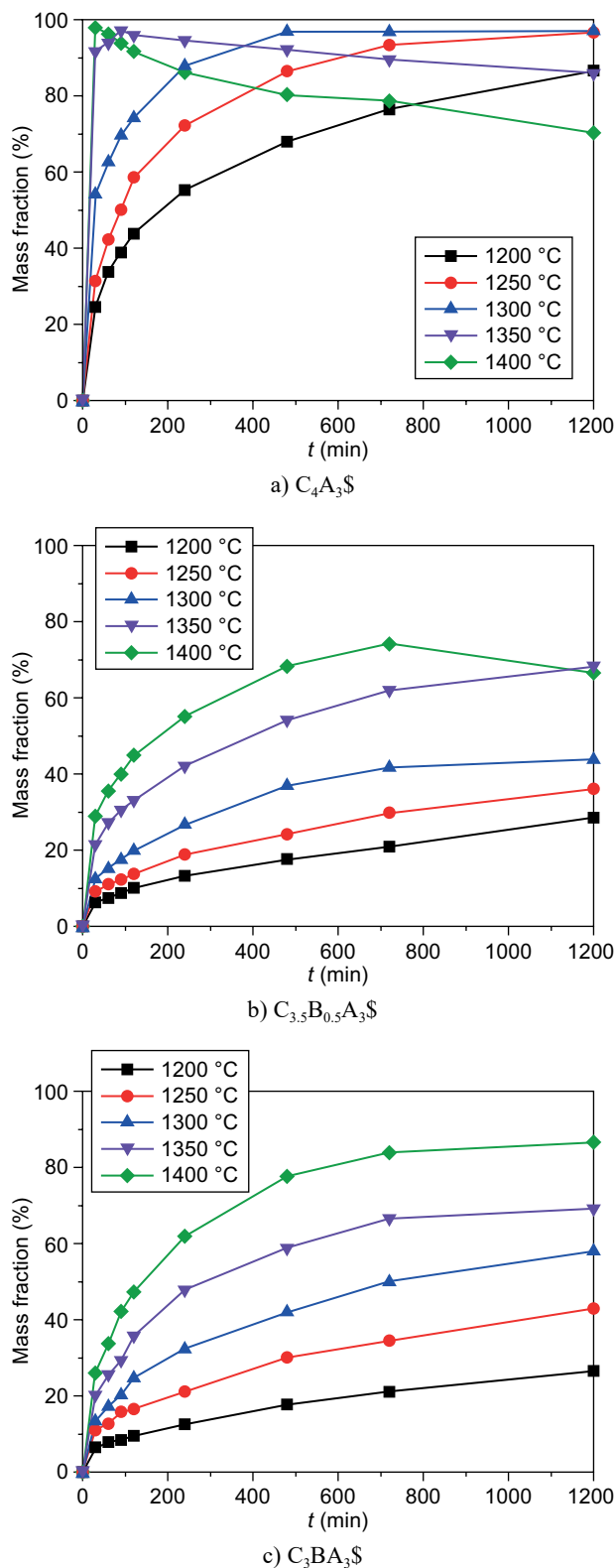


Figure 3. The conversion rate of the $C_{4-x}B_xA_3$ minerals. (Continue on next page)

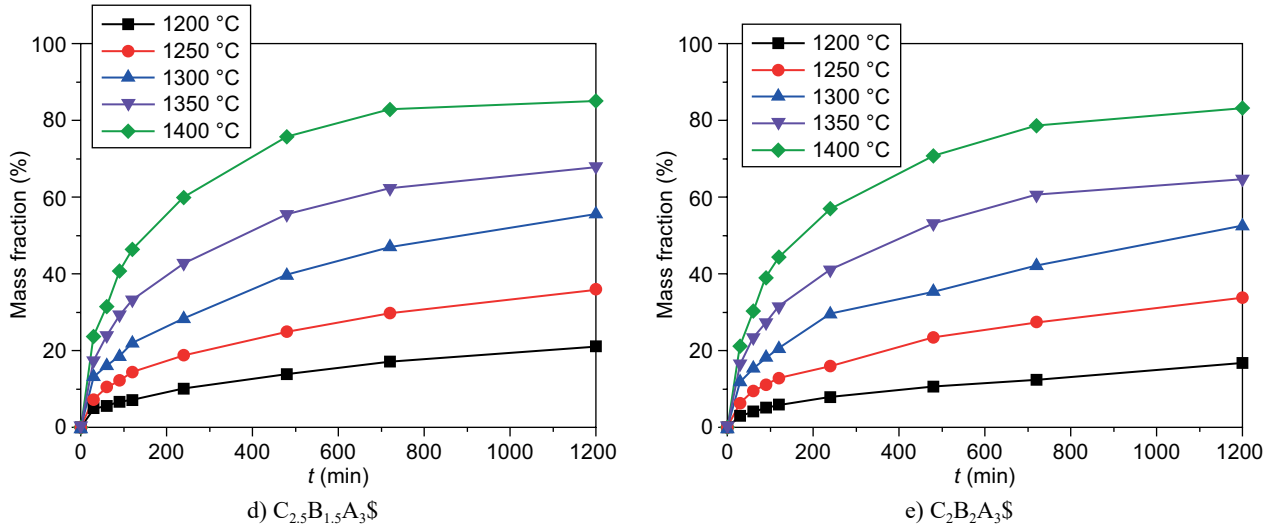


Figure 3. The conversion rate of the $C_{4-x}B_xA_3$ minerals (figs. 3a-e represent the conversion rate of C_4A_3 , $C_{3.5}B_{0.5}A_3$, C_3BA_3 , $C_{2.5}B_{1.5}A_3$, $C_2B_2A_3$, respectively).

under the same calcination conditions. It is easy to come to the conclusion that the $C_{4-x}B_xA_3$ formation becomes increasingly difficult with an increase in the Ba-doping concentration. Since the radius of Ba^{2+} (135 pm) is much larger than that of Ca^{2+} (100 pm), it is easy to understand that it requires much more energy to form Ba-doped ye'elimite. A similar conclusion is also reported with the aluminate minerals. The formation activation energy of the Ba-doped aluminate (about $286.92 \text{ kJ}\cdot\text{mol}^{-1}$) is higher than the stoichiometric one (about $197.76 \text{ kJ}\cdot\text{mol}^{-1}$) [43]. Another difference is that there is no significant decomposition phenomenon among the $C_{4-x}B_xA_3$ minerals, except $C_{3.5}B_{0.5}A_3$ at $1400 \text{ }^\circ\text{C}$. It can be illustrated that the Ba^{2+} substitution at the Ca^{2+} -site in C_4A_3 can significantly enhance its thermal stability, which is also reported elsewhere [20]. The reason can be explained by the difference in the bond dissociation energies between Ba–O ($562 \pm 13.4 \text{ kJ}\cdot\text{mol}^{-1}$) and Ca–O ($383.3 \pm 5.0 \text{ kJ}\cdot\text{mol}^{-1}$) [41].

The formation kinetics model of the $C_{4-x}B_xA_3$ minerals

In this part, appropriate kinetics models are discussed and selected to study the effect of the Ba-doping concentration on the $C_{4-x}B_xA_3$ formation process. The key to selecting the kinetics models is primarily based on the statistical fitting of the mathematical models by the evaluation of the correlation coefficient (R^2) values and the standard deviation [42]. Notably, the decomposition points (such as the points of C_4A_3 at $1300 \text{ }^\circ\text{C}$, $1350 \text{ }^\circ\text{C}$ and $1400 \text{ }^\circ\text{C}$ in Figure 3a) are not taken into consideration in this study. All of the to-be-assessed models [42, 43] are listed in Table 4. They can be summarised by the function $f(\alpha) = K_{(T,C)} t + C$, where K is the rate constant and ' α ' represents the mass fraction of $C_{4-x}B_xA_3$ at a certain sintering duration (abbr. ' t ' in the above equation). The results show that the highest R^2 values (Table 5) are yielded from the Jander model, where the standard deviation is also the minimum. Therefore, the Jander model is selected to perform the kinetic calculation in the following work. The relationship

Table 4. The solid-state reaction and kinetic models.

Equation number	Kinetics equation	Reaction mechanism	Kinetics model
D ₁	$D_1 = \alpha^2 = K_T t$	One-dimensional diffusion mechanism	Flat model
D ₂	$D_2 = (1 - \alpha)\ln(-\alpha) + \alpha = K_T t$	Two-dimensional diffusion mechanism	Cylindrical model
D ₃	$D_3 = [1 - (1 - \alpha)^{1/3}]^2 = K_T t$	Three-dimensional diffusion mechanism	Jander equation
D ₄	$D_4 = 1 - 2\alpha/3 - (1 - \alpha)^{2/3} = K_T t$	Three-dimensional diffusion mechanism	Ginstling equation
R ₁	$R_1 = -\ln(1 - \alpha) = K_C t$	Interfacial chemical	Spherical model (first order reaction)
R ₂	$R_2 = 1 - (1 - \alpha)^{1/2} = K_C t$	Interfacial chemical	Cylindrical model (second order reaction)
R ₃	$R_3 = 1 - (1 - \alpha)^{1/3} = K_C t$	Reaction mechanism	Spherical model (third order reaction)

curves of $f(\alpha)-K_{(T,C)}t$ of the $C_{4-x}B_xA_3$ minerals are shown in Figure 4a-e, respectively.

After the linear fitting of time and $f(\alpha)$, the reaction rate constants, i.e., the k value, which quantitatively represents the chemical reaction velocity and changes with temperature can be obtained by the calculated slopes. The reaction rate constants with the different

Ba-doping concentration and temperature are depicted in Figure 5. The chart illustrates that the constant k gradually increases with the rise in the temperature for the same mineral. Another phenomenon is that it shows a general decline with an increase in the Ba-doping concentration. However, one singular point, where the Ba-doping concentration appears to be 0.5, shows

Table 5. The result of the linear regression analysis.

Equation number	The average value of R^2				
	C_4A_3	$C_{3.5}B_{0.5}A_3$	C_3BA_3	$C_{2.5}B_{1.5}A_3$	$C_2B_2A_3$
D ₁	0.7162	0.9694	0.9582	0.9713	0.9779
D ₂	0.8410	0.9831	0.9768	0.9858	0.9898
D ₃	0.9942	0.9932	0.9896	0.9953	0.9960
D ₄	0.9466	0.9872	0.9823	0.9901	0.9929
R ₁	0.8458	0.8941	0.8946	0.9226	0.9332
R ₂	0.8788	0.8513	0.8476	0.8820	0.8959
R ₃	0.9315	0.8664	0.8646	0.8971	0.9095
Standard deviation of D ₃	0.005508	0.005059	0.0075	0.002854	0.002513

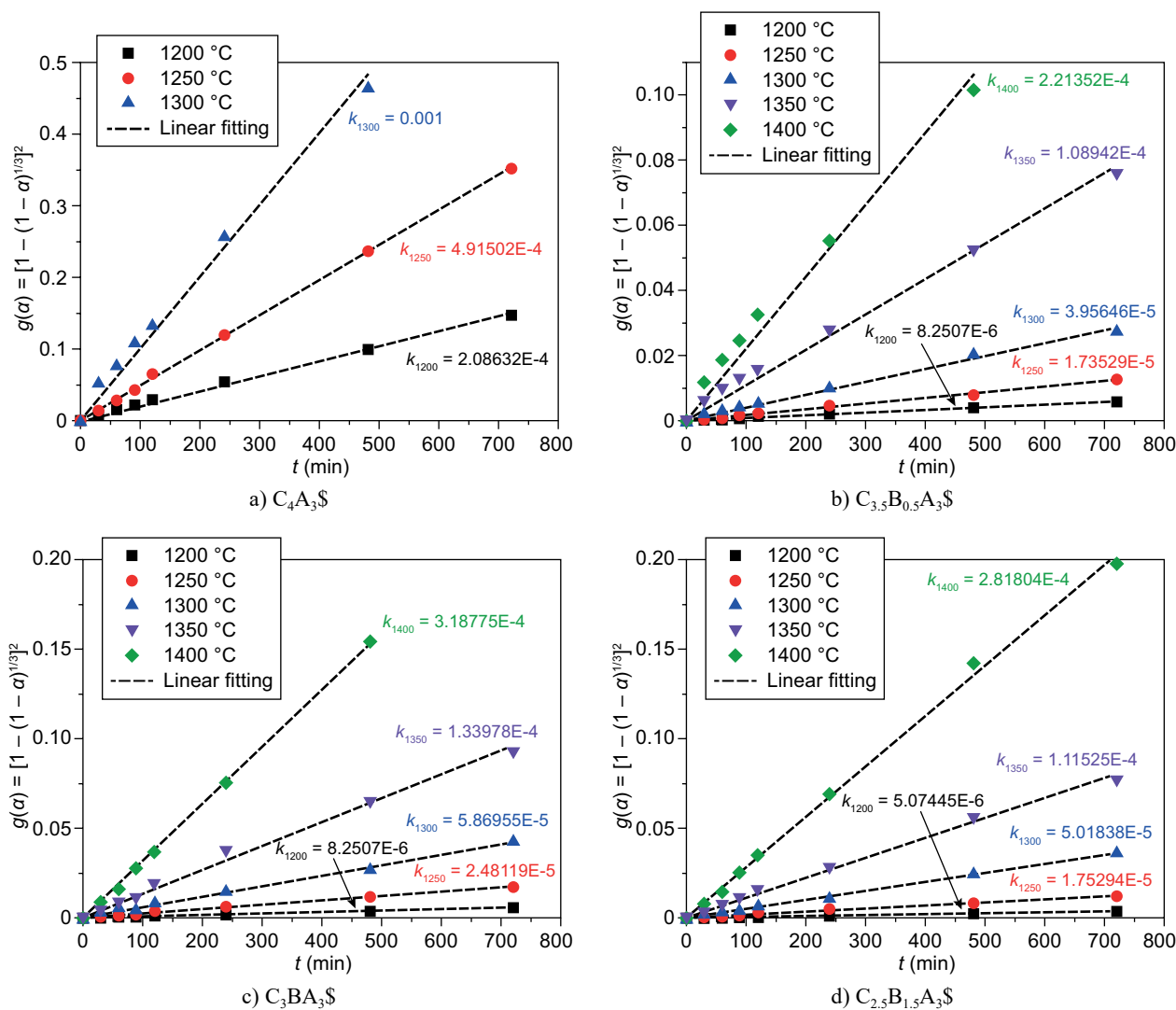


Figure 4. The relationship curves of $f(\alpha)-K_{(T,C)}t$ of the $C_{4-x}B_xA_3$ minerals (Figs. 4a-e represent the linear regression results of C_4A_3 , $C_{3.5}B_{0.5}A_3$, C_3BA_3 , $C_{2.5}B_{1.5}A_3$, $C_2B_2A_3$, respectively). (Continue on next page)

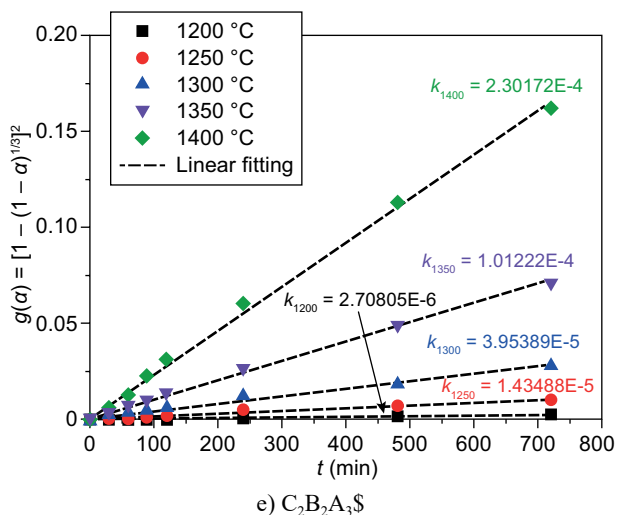


Figure 4. The relationship curves of $f(\alpha)-K_{(T,C)}$ of the $C_{4-x}B_xA_3$ minerals.

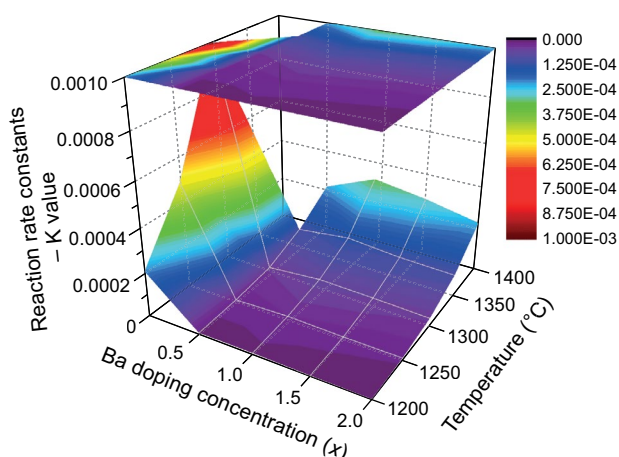


Figure 5. The reaction rate constants with the different Ba-doping concentrations and sintering duration.

a lower ‘ k ’ value than expected. This phenomenon is more obvious under the conditions of a higher temperature. As discussed above, it is probably caused by the sulfur volatilised from the $CaSO_4$ decomposition, restricting the formation of ye’elimite. When the Ba-doping concentration is larger than 1.0 ($C_{4-x}B_xA_3$, $x > 1$), the $BaSO_4$ produced as the main sulfate-containing mesophase with a higher decomposition temperature will play an important role in the sulfur solidification.

The apparent activation energy

The apparent activation energy (E_a) which could reflect the difficulty of the solid-state reaction, is the minimum energy required for the molecules to be converted to the active chemical component from the normal reactive states [20, 24, 31, 38, 39, 44]. E_a can be calculated from the Arrhenius equation (Equations 11-12) as follows,

$$k = Ae^{-(E_a/RT)} \tag{11}$$

$$\ln k = \ln A - (E_a/RT) \tag{12}$$

where A is the pre-exponential factor, R represents the ideal gas constant ($8.314 \times 10^{-3} \text{ kJ}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$), ‘ T ’ indicates the reaction temperature (k), respectively.

The linear fitting relation between $\ln k$ and $-1/RT$ is shown in Figure 6 and the corresponding E_a values are reported in Table 6. Obviously, it gradually increases with an increase in the Ba-doping concentration. A fitting analysis, seen in Figure 7, depicts that the E_a (y)

Table 6. The apparent activation energy of the $C_{4-x}B_xA_3$ minerals.

Ba-doping concentration	$x = 0$	$x = 0.5$	$x = 1$	$x = 1.5$	$x = 2$
E_a (kJ·mol ⁻¹)	302.158	344.472	370.451	405.939	446.194

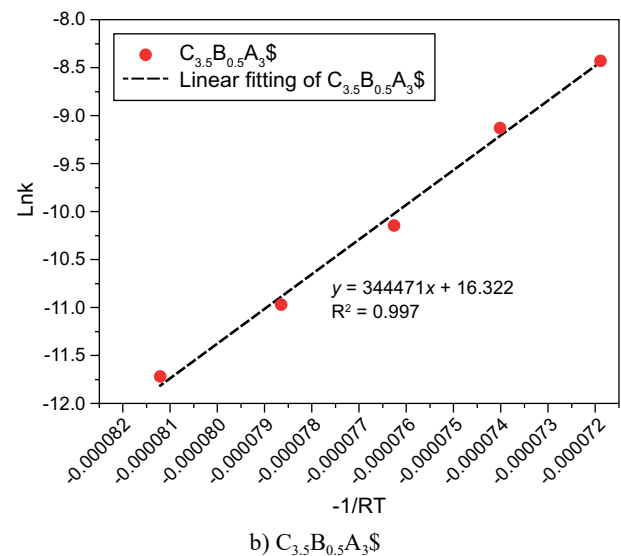
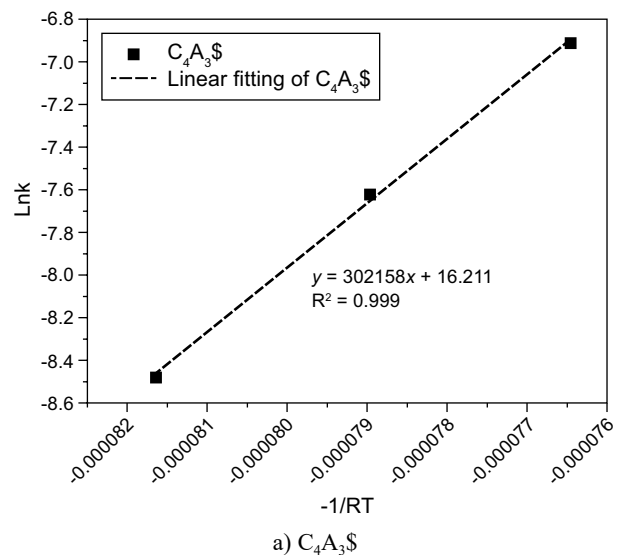


Figure 6. The Arrhenius equation fitting the results of the $C_{4-x}B_xA_3$ minerals. (Continue on next page)

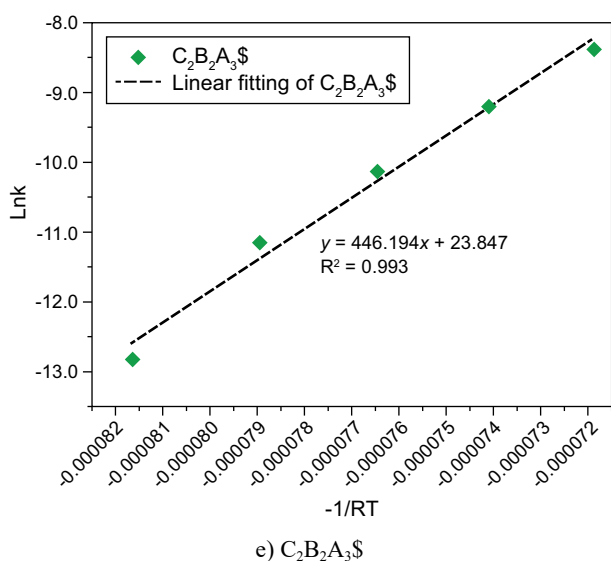
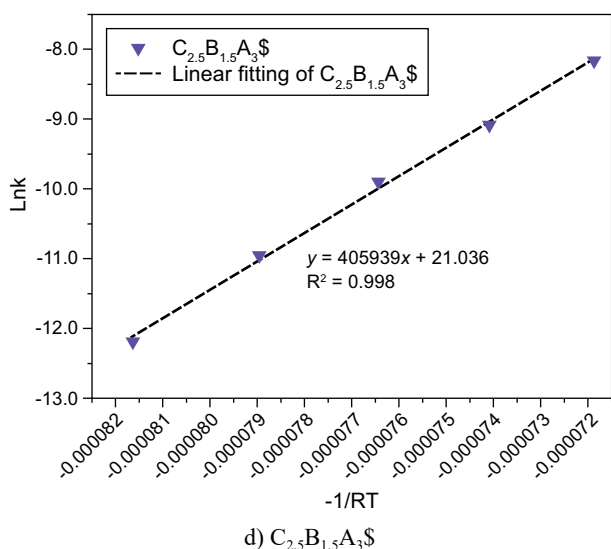
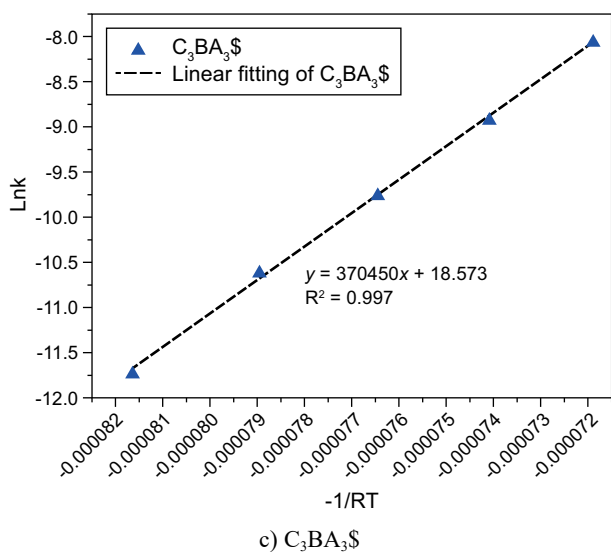


Figure 6. The Arrhenius equation fitting the results of the $C_{4-x}B_xA_3$ minerals.

and the Ba-doping concentration (x) can be well imitated with ' $y = 71.9x + 304$ '. The goodness of the fit is as high as 0.992. A previous study has reported that the activation energy of the Ba-doped ye'elinite formation is larger than the stoichiometric one [20]. Here, we demonstrate that ' E_a ' has approximately linear growth with the amount of barium incorporation content. Li [29] proposed that C_4A_3 formed originally from the basic 'Al-O' skeleton structure and then the ions of Ca^{2+} and SO_4^{2-} diffused into the crystal structure. Compared with Ca^{2+} , it is more difficult for Ba^{2+} to enter into the above skeleton structure, due to its larger ionic radius, to form the Ba-doped ye'elinite. So, it is easy to understand that the more barium that is doped, the higher energy barrier needs to be overcome. Therefore, it makes a higher impurity phase formed at the low sintering temperature, which is consistent with the Rietveld results above (Table 3).

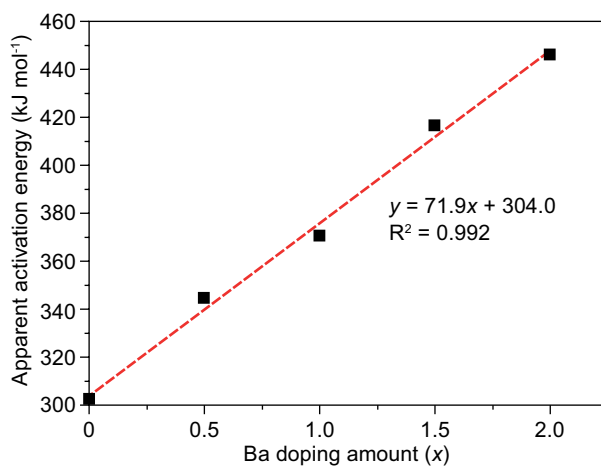


Figure 7. The relationship curves between the apparent activation energy and the Ba-doping concentration.

CONCLUSIONS

In this work, the solid-state reaction process of $C_{4-x}B_xA_3$ minerals with different Ba-doping concentrations ($x = 0, 0.5, 1, 1.5$ and 2) have been studied. The effect of the Ba-doping concentration on the formation kinetics is systematically discussed. The results above lead us to draw the following conclusions:

- $BaSO_4$ is the essential intermediate phase for the formation of Ba-doped ye'elinite. The solid-state reaction processes of $C_{4-x}B_xA_3$ are proposed as two main forms, corresponding to the cases in which the Ba-doping concentration (x) is larger than and less than "1", respectively. The same point is that the $BaSO_4$ is the basis of the formation of the Ba-doped ye'elinite. When $x > 1$, the different point is that the excess BaO continues to form the $BaAl_2O_4$ mineral with Al_2O_3 .
- The Jander diffusion model shows the optimal fitting

for a series of $C_{4-x}B_xA_3S$ minerals. An obvious linearity rising relationship exists between the apparent activation energy (E_a) and the Ba-doping concentration (x). A linear equation was obtained with a fitting goodness of 0.992.

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